

ELECTROCHEMICAL pH CONTROL FOR THE PROCESS OF METALS RECOVERY FROM WASTE PRINTED CIRCUIT BOARDS



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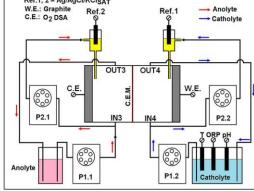
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INTRODUCTION

The waste printed circuit boards (WPCBs) represent only 3-5% from the global amount of waste electric and electronic equipment (that will exceed 50 Mt in 2018 [1]), but concentrate more than 40% from the value of the recoverable metals [2]. Therefore, pyrometallurgical, hydrometallurgical and physico-mechanical processes were developed for metals recovery from WPCBs (MRWPCBs), all of them being energy intensive and/or highly polluting [3]. Our preliminary results [4] revealed that the electrochemical MRWPCBs based on the Br₂/KBr leaching system represents an economical and eco-friendly recycling alternative, but requires a carefully pH control in order to avoid the precipitation of the dissolved metals.

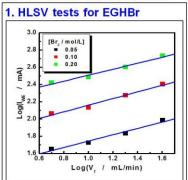
Study of the on-site electro-generation of HBr (EGHBr) as pH adjusting agent and of Br2 (EGBr2) as raw material for EGHBr in order to avoid the permanent addition/consumption of fresh reagents.

EXPERIMENTAL SETUP AND CONDITIONS Ref.1, 2 = Ag/AgCI/KCISAT



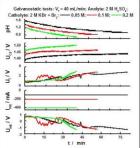
- ✓ Electrochemical cell: MicroFlowCell® divided filter-press reactor (DFPR) equipped with Nafion® 324 membrane and PVC tubes Luggin capillaries;
- Experimental techniques: Hydrodynamic linear scan voltammetry (HLSV) @ 5 mV/s; Galvanostatic/potentiostatic EGHBr and EGBr₂ tests; Computer controlled automatic titration of HBr and Br2 with 0.1 N KOH and 0.1 N Na2S2O3.
- ✓ Working electrode (W.E.): Graphite bloc of 10 cm² active area (A.A.);
- Counter electrodes (C.E.): DSA-O₂ & Ni for EGHBr & EGBr₂, respectively (10 cm² A.A.);
- √ Reference electrodes (Ref.): Ag/AgCI/KCI_{SAT};
- ✓ Anolytes: 2 M H₂SO₄ and 2 M KBr for EGHBr and EGBr₂, respectively;
- Catholytes: For EGHBr & HLSV: 2 M KBr + 0.05, 0.1 and 0.2 M Br₂; For EGHBr: leaching solution (2 M KBr + 0.08 M FeBr₃ + 0.16 M CuBr₂ + 0.1 M Br₂); For EGBr₂: 0.1 M KOH;
- Equipments: Computer interfaced: P/G-stat DXC236 (Datronix Computers, Romania); Peristaltic pumps Reglo-Analog & Reglo-Digital (Ismatec, Switzerland); Insulated highimpedance voltmeters C863 (Consort, Belgium).

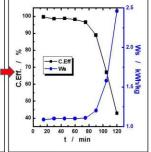
RESULTS AND DISCUSSIONS



 \bigcirc In the used V_{f} range, a 0.35 slopes mean value for the Log(IWE) Log(V_f) linear correlations indicates a turbulent flow of "thin layer" type.

2. Galvanostatic and potentiostatic EGHBr tests





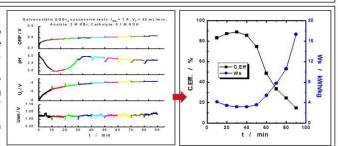
- lacktriangle In galvanostatic mode, high values of l $_{
 m WE}$ induce fast decrease of U $_{
 m WE}$, favoring H $_2$ evolution (HE).
- The presence of the Fe²⁺/Fe³⁺ and Cu⁺/Cu²⁺ redox coupes in catholyte and the potentiostatic process control allow the EGHBr with diminished occurrence of HE.
- ⇒ The final pH value of ~0.3 is adequate for the successful leaching of base metals from WPCBs.
- The current efficiency (C.Eff.) and specific energy consumption (Ws) for the EGHBr process present acceptable values for obtained HBr concentrations less than 0.5 M.

3. Galvanostatic EGBr₂ tests

In order to avoid the handling of the extremely toxic and corrosive liquid Br2, studies concerning its in-situ EGBr2 are also performed in the DFPR equipped with electrodes on graphite and Ni as anode and cathode, respectively.

The C.Eff. and Ws for the EGBr₂ process preserve acceptable values for resulting Br₂ concentrations less than 0.1 M. This value determines a high efficiency for the EGHBr process and an ORP of around +0.8 V, highly enough to assure the base metals leaching from WPCBs.

Simultaneously with the EGBr₂ process, a concentrated solution of KOH is generated, useful for the metals ions separations.



CONCLUSIONS

- Controlling adequately the operational parameters, HBr can be efficiently generate electrochemically in-situ and used as pH control agent during the electrochemical process of metals recovery from WPCBs.
- The electrochemical oxidation of bromide to bromine in a divided filter-press reactor offer a reliable raw material source for the EGHBr process and generate additionally a concentrate alkaline solution useful for the leached metals ions separation.

ACKNOWLEDGEMENT

This work was supported by a grant of the Romanian Ministry of Research and Innovation, CCCDI - UEFISCDI, project number PN-III-P1-1.2-PCCDI-2017-0652 / 84PCCDI / 2018, within PNCDI III

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